

Online Control of Spray Cooling Using CONONLINE

Control System Design & Performance

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Outline

- Project overview
- CONONLINE Development
 - Software sensor
 - Monitor
 - Controller
- Setpoint generation
- Example simulation
- Ongoing work

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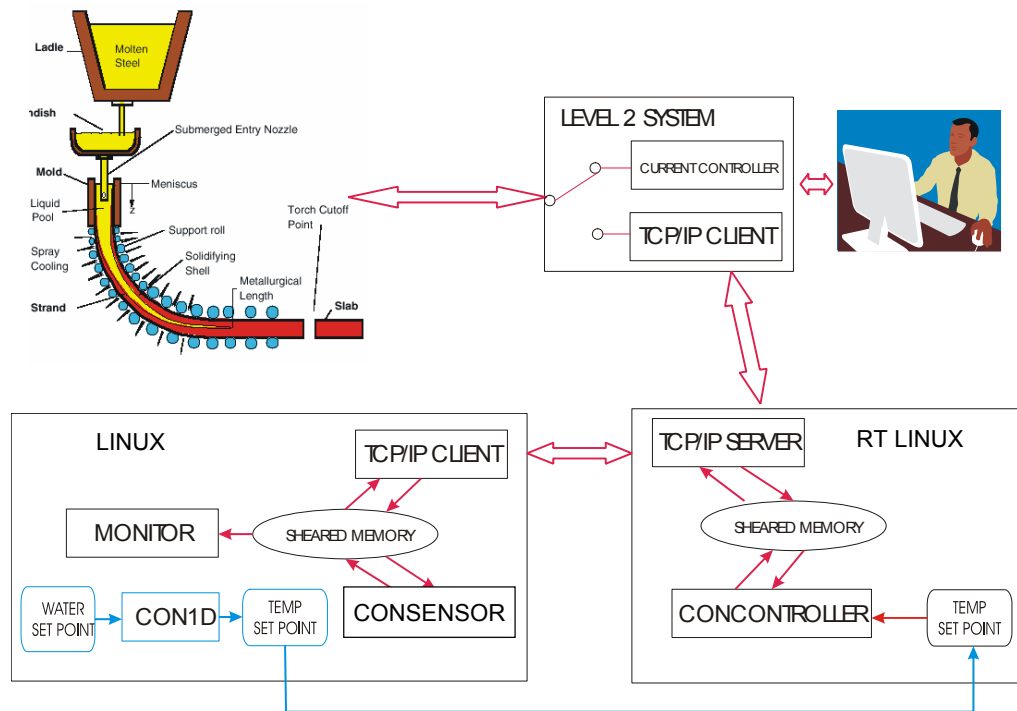
Approaches to Secondary Cooling Control

- 1) Manual control:**
 - Operator sets of water flow rates
 - Difficult at high casting speeds when response times must be short
- 2) Casting-speed-based control:**
 - Set water flow rates according to casting speed
 - Results in non-optimal cooling during transient conditions
- 3) New Software-sensor-based control:**
 - Create “software sensor,” an accurate, real-time computational model to base control on
 - Conventional feedback control has not yet been successfully implemented due to unreliability of optical pyrometer sensors.

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System Overview



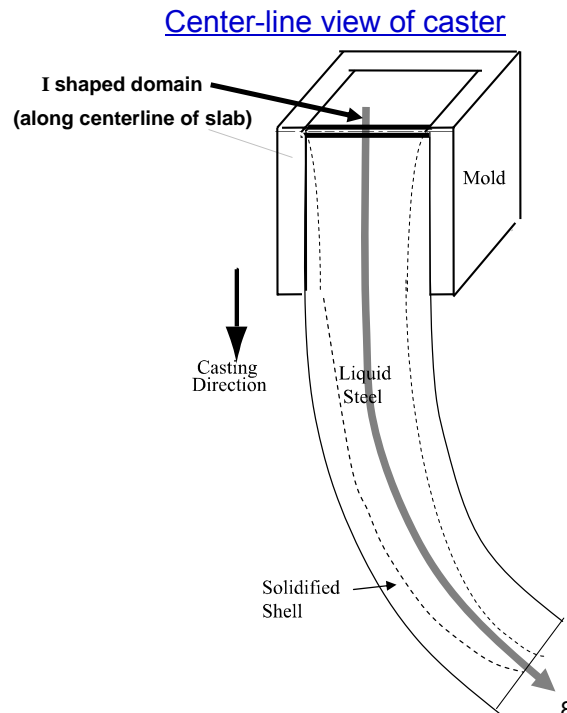
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CON1D: Overview

- Fundamentally based transient finite-difference model:

$$\rho_{steel} C_{p, steel} \frac{\partial T}{\partial t} = k_{steel} \frac{\partial^2 T}{\partial x^2} + \frac{\partial k_{steel}}{\partial T} \left(\frac{\partial T}{\partial x} \right)^2$$

- CON1D predicts:
 - shell thickness
 - temperature distribution
 - total heat removal
 - heat flux profiles
 - mold water temperature rise (to match measurements)

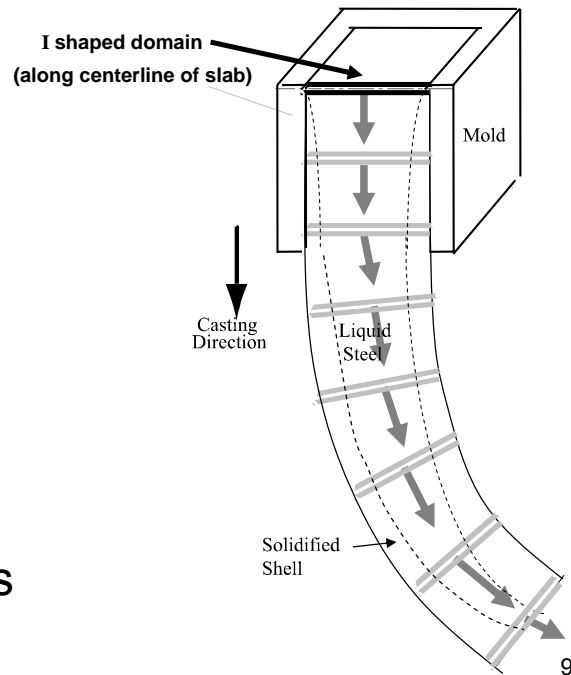


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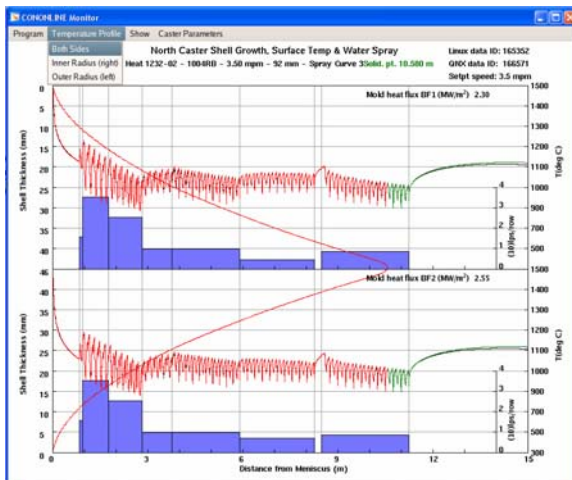
CON1D: Application

- CON1D program:
 - runs through entire caster in ~ 0.5 s
 - predicts temperature and other phenomena for only one slice at a time
 - we need the temperature profile of the whole slab
- Solution: multiple slices

Center-line view of caster



CONONLINE Display



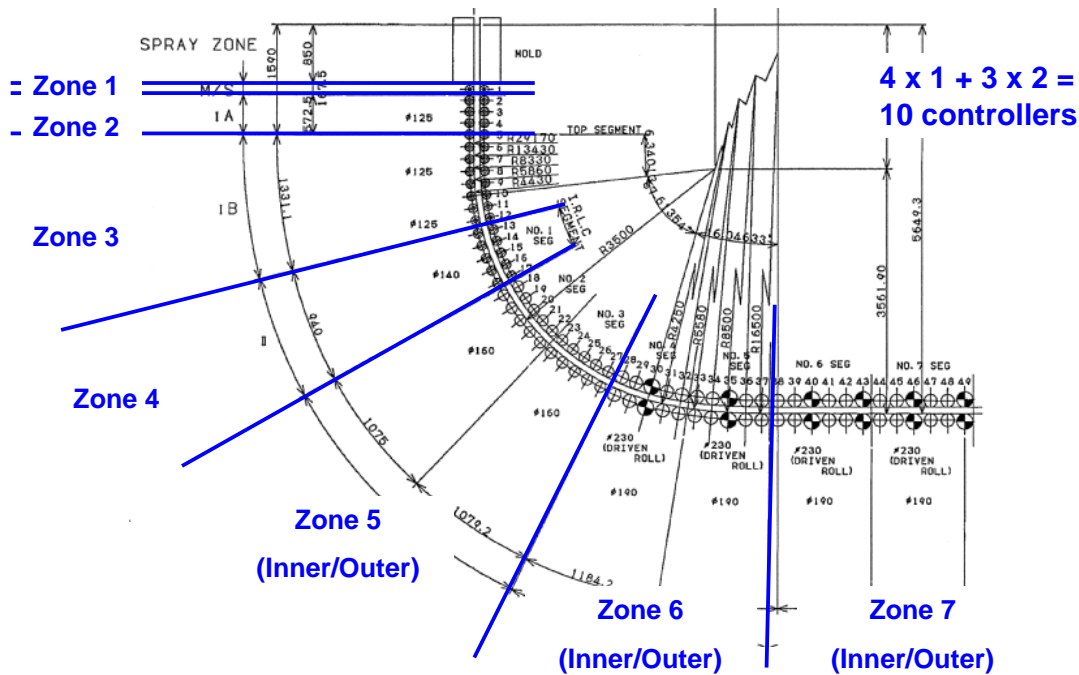
CONONLINE Monitor

Program: Temperature Profile Show: Caster Parameters

North Caster Parameters

Running mode	-1	Mold heat flux BF1 (MW/m ²)	2.30	Carbon, %	0.0400
Caster mode	1	Mold heat flux BF2 (MW/m ²)	2.55	Manganese, %	0.3700
Spray water pattern	3	Mold heat flux BF3 (MW/m ²)	2.55	Sulfur, %	0.0050
cast. in prog.	1	Mold heat flux BF2 (MW/m ²)	2.55	Phosphorus, %	0.0050
cast. tailing	1	Mold water steel grade	9.0000	Silicon, %	0.0100
liquid core reduct.	1	Mold water inlet grade	9.0000	Chromium, %	0.0440
cast length	12340.00	Mold water inlet T (deg C)	43.00	Nickel, %	0.0430
Casting speed (m/min)	3.50	Mold water outlet T BF1 (deg C)	33.12	Copper, %	0.1320
Caster width (mm)	1396.00	Mold water outlet T BF2 (deg C)	33.12	Molybdenum, %	0.0110
Caster thickness (mm)	92.00	Mold water outlet T BF3 (deg C)	33.12	Titanium, %	0.0030
Tundish temperature (deg C)	1553.00	Mold water outlet T HF1 (deg C)	33.12	Aluminum, %	0.0360
Tundish temp. sup. M. (deg C)	1553.00	Mold water outlet T HF2 (deg C)	33.12	Vanadium, %	0.0020
Tundish weight (ton)	2.00	Mold water delta T BF1 (deg C)	-9.88	Nitrogen, %	0.0000
Spray water inlet T (deg C)	25.0000	Mold water delta T BF2 (deg C)	-9.88	Hotmetal, %	0.0010
Nozzle submerg. depth (mm)	150.00	Mold water delta T HF1 (deg C)	-9.88	Tungsten, %	0.0000
Heat ID	1232-02	Mold water delta T HF2 (deg C)	-9.88	Add. weight 1, %	0.0000
Grade	100410	Mold water delta T HF3 (deg C)	-9.88	Add. weight 2, %	0.0000
				Add. weight 3, %	0.0000
				Add. weight 4, %	0.0000
				Add. weight 5, %	0.0000
				Add. weight 6, %	0.0000
				Add. weight 7, %	0.0000
				Add. weight 8, %	0.0000
				Add. weight 9, %	0.0000
				Add. weight 10, %	0.0000

Caster



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Controller Design

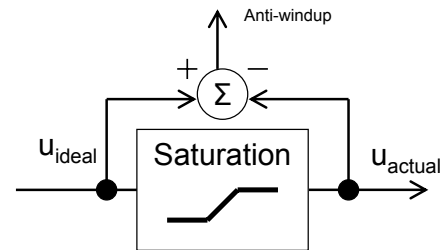
- Zone-based design: 10 subcontrollers, one for each spray zone
- Controller Algorithm:** At each second of time:
 - Obtain surface temperature profile from CONONLINE.
 - For all 10 zones:
 - Compute the zone-based surface temperature average T_{avg} for current zone. And form the tracking error $T_{err} = T_{avg} - T_{sp}$
 - Use T_{err} to compute the water flow rate command = $Nominal_flow + \Delta flow(t)$,

$$\Delta flow(t) = k_p T_{1err}(t) + k_i \int_0^t T_{1err}(s) ds$$
 - Send all water flow rate commands to CONONLINE, Caster, and Monitor

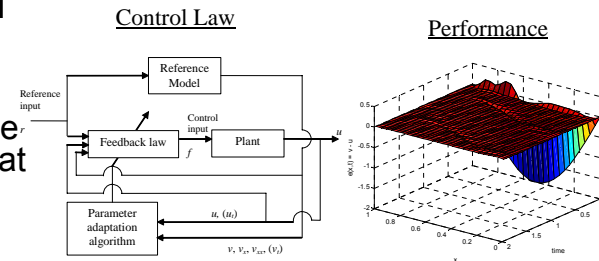
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Improvements to Controller

- Anti-windup
 - Actuator saturation can lead to windup of integral controller
 - Simple anti-windup scheme added



- Optimal/Adaptive control law development
 - In progress
 - Adaptive control laws have been designed for 1-D heat equation with spatially varying parameters



- Metallurgical length (ML) control

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Transient ML Control

- Prevent overshoot of metallurgical length (ML):
 - A small amount of ML overshoot (0.1m) results under good temperature control
 - Can trade the performance of temperature control for metallurgical length control by **temperature setpoint conditioning**
 - Requires steady state ML within bounds
 - For 6th, and 7th spray zones, $T_{sp_c} = T_{sp} \cdot (1 - drop)$
 - $drop = c_1 \cdot (v_{solidpt})^{c_2} \cdot (z_{solidpt} - c_3)^{c_4}$

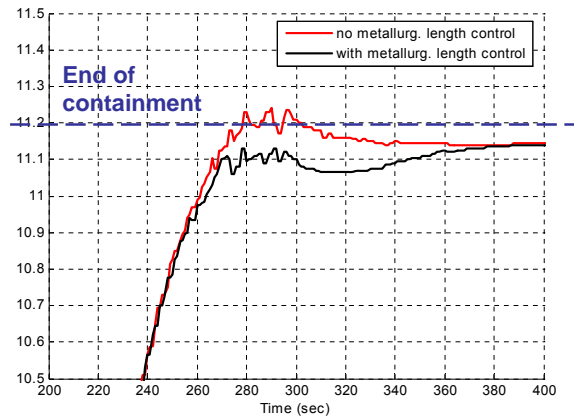
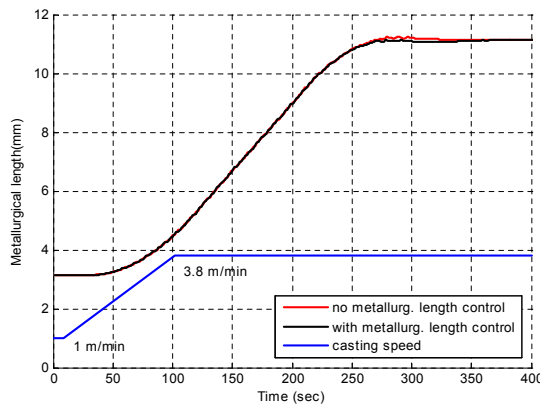
$$\text{if } \begin{cases} v_{solidpt} > 0 \text{ and} \\ z_{solidpt} - c_3 > 0 \end{cases}$$

$$\text{else, } drop = 0$$

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Transient ML Control: Performance

- Metallurgical length overshoot eliminated



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Intelligent ML Control

- Transient control depends on setpoints being “safe” conditions
- Open problem: ensuring metallurgical length behavior automatically
 - Conflict between setpoint tracking and metallurgical length tracking?
 - “Envelope” for system: known safe running conditions hard-coded into controller?
 - Moving boundary control of Stefan problem?

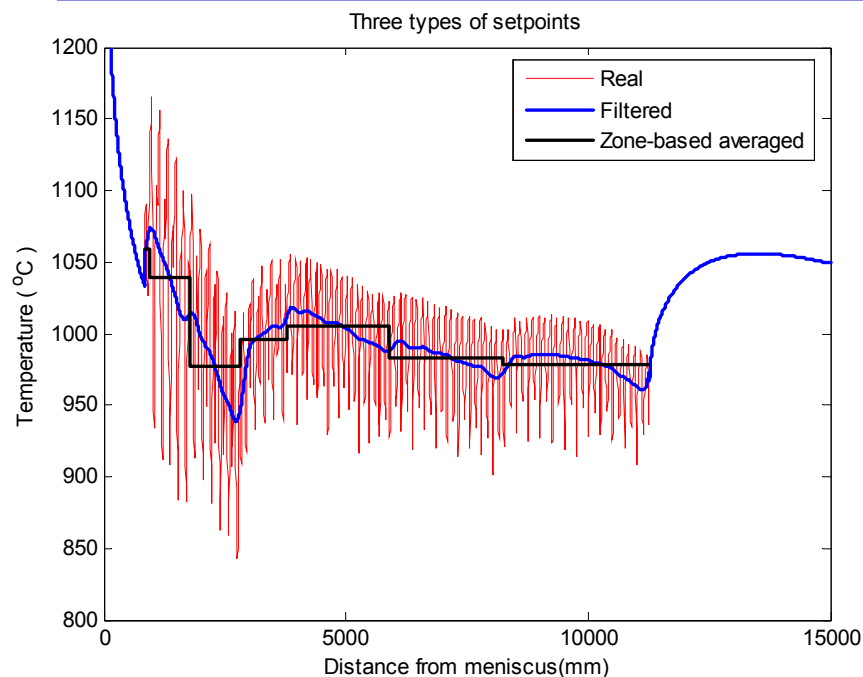
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Setpoint Generation

- From Nucor: spray water flow rate set points
 - Empirically based, from past experience
 - Casting-speed-dependent
- Convert to surface temperature profiles
 - Output from CON1D becomes temperature setpoint
 - Conditions:
 - 9 Casting speeds
 - 8 Spray patterns

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Temperature setpoints



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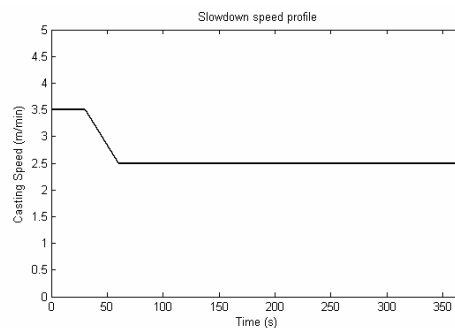
Problems With Setpoints

- Type of setpoints
 - Should setpoints be based off spray tables or desired temperature profiles?
- Casting speed variations
 - Should different speeds have different temperature profiles?
- Mold heat flux variations
 - Setpoint generator assumes heat flux equal to standard conditions (eg from Ciccuti et al)

$$Q_c = 4.63 \cdot 10^6 \mu^{-0.09} T_{flow}^{-1.19} T_C^{0.47} \left\{ 1 - 0.152 \exp \left[- \left(\frac{0.107 - \%C}{0.027} \right)^2 \right] \right\}$$
 - But, in practice, mold heat flux may vary
 - How should model compensate?

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Simulation: Sudden Slowdown

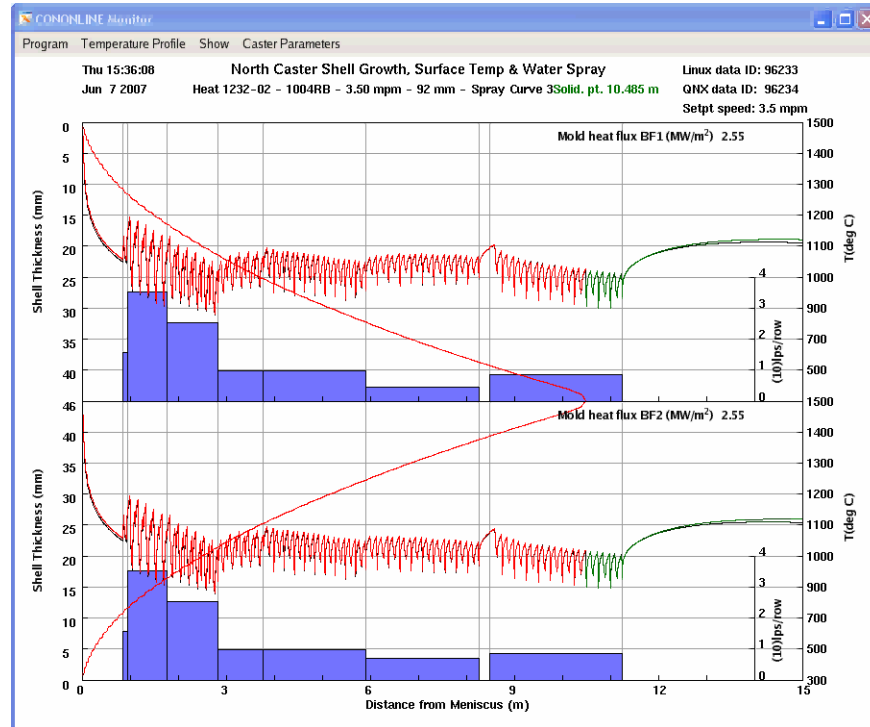


- Compare
 - Casting-speed-based controller: setting water flow rate proportional to casting speed
 - Model-based PI controller: speed-proportional setpoints
 - Model-based PI controller: speed-independent setpoints

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Slowdown: Casting-speed-based Controller

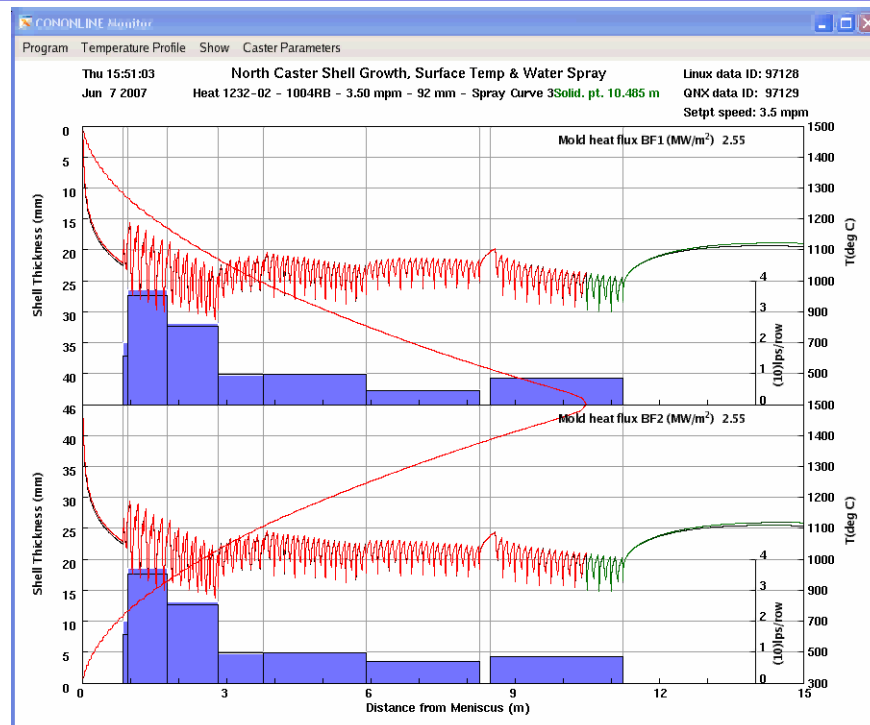
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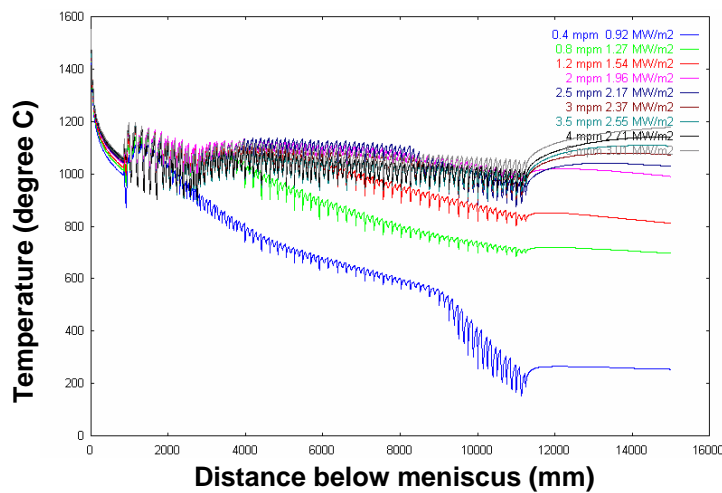
Slowdown: PI Controller, Speed-dependent Setpoints

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Casting Speed

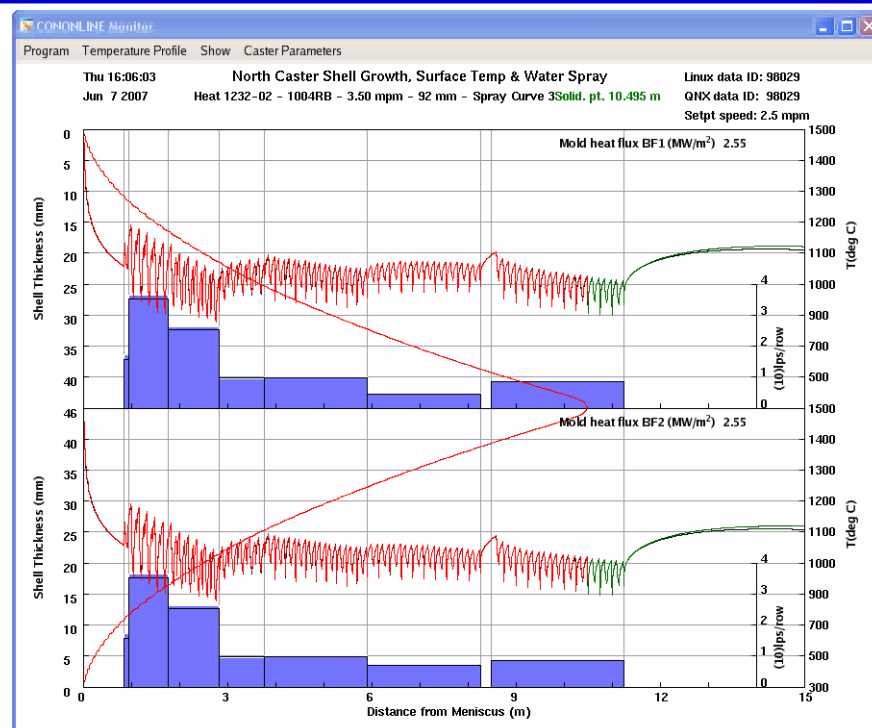


- For 2 – 5 m/min, temperature setpoints are approximately constant
- Suggests that constant temperature setpoint is desired
- Take representative casting speed as setpoint for all casting speeds

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Slowdown: PI Controller, Speed-independent Setpoints

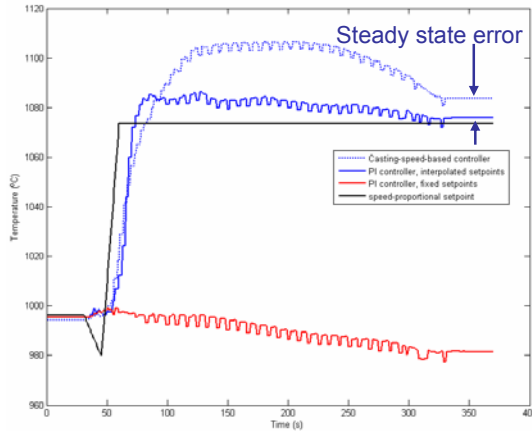
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Slowdown: Comparison

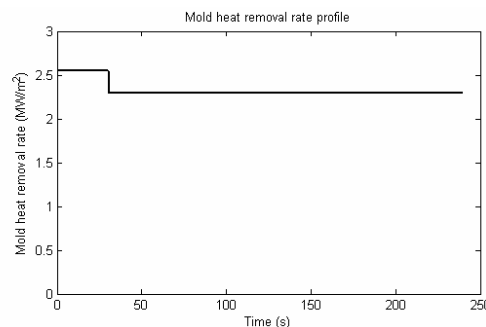
Inner radius surface temperature at end of containment



- Casting-speed-based controller causes temperature overshoot
- Transient behavior is tracked closer with model-based controllers
- Steady-state error is caused by mold heat removal rate variations

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Simulation: Mold Heat Removal Rate Drop

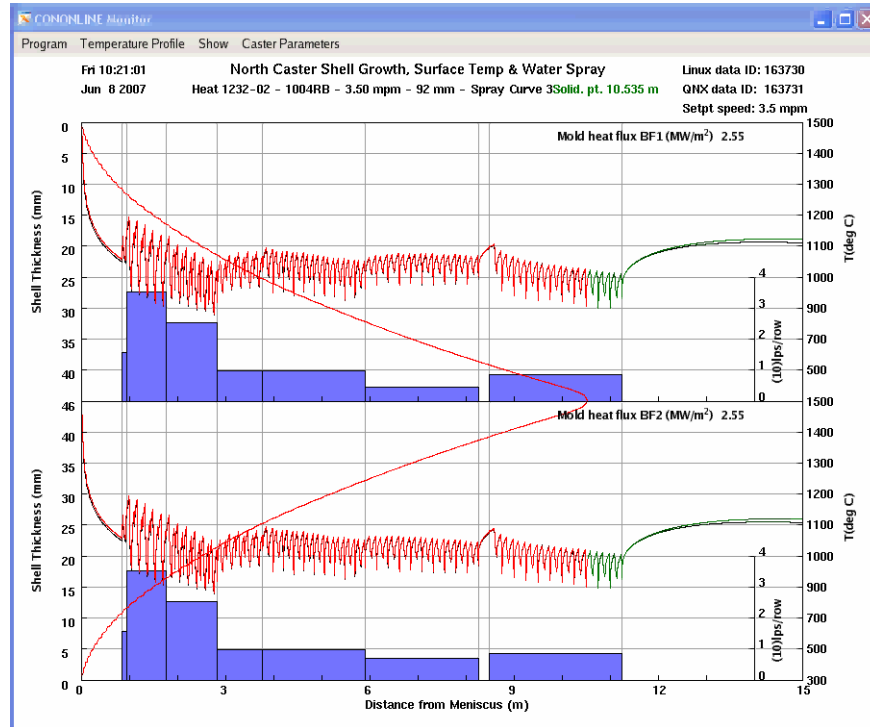


- Mold heat removal rate (MHRR) on inner radius, broad face drops 10% at 30 seconds
- Compare
 - Casting-speed-based controller: setting water flow rate proportional to casting speed
 - Model-based PI controller: Fixed setpoints
 - Model-based PI controller: Mold-exit-temperature-dependent setpoints

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MHRR Drop: Casting-speed-based Controller

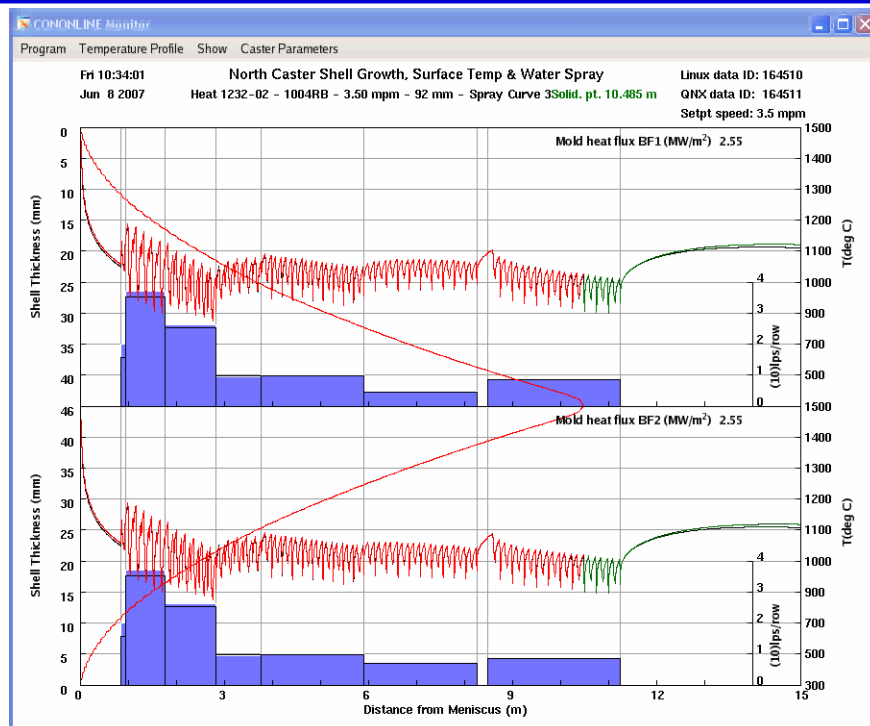
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MHRR Drop: PI Controller, Fixed Setpoints

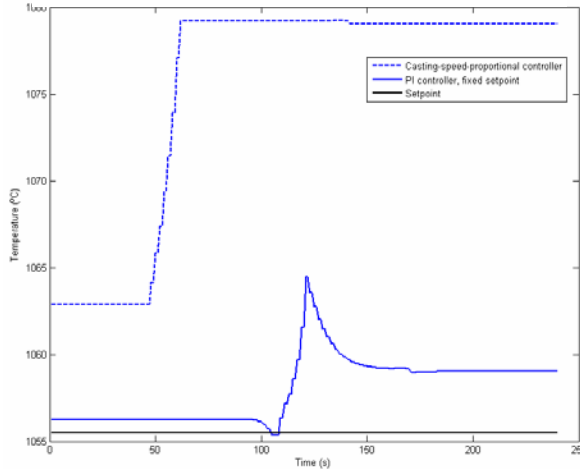
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Mold Heat Removal Rate Drop: Comparison

Inner radius surface temperature at
end of 3rd spray zone

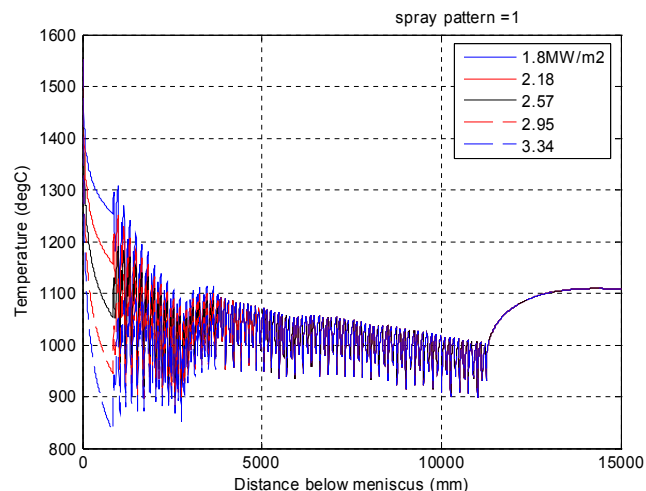


- Fixed setpoint controller tries to hold temperature constant despite change in mold exit temperature
- Can overcool strand and create detrimental transients in top regions of caster – even worse if mold heat flux varies continuously

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Vary Setpoints with Mold Exit Temperature

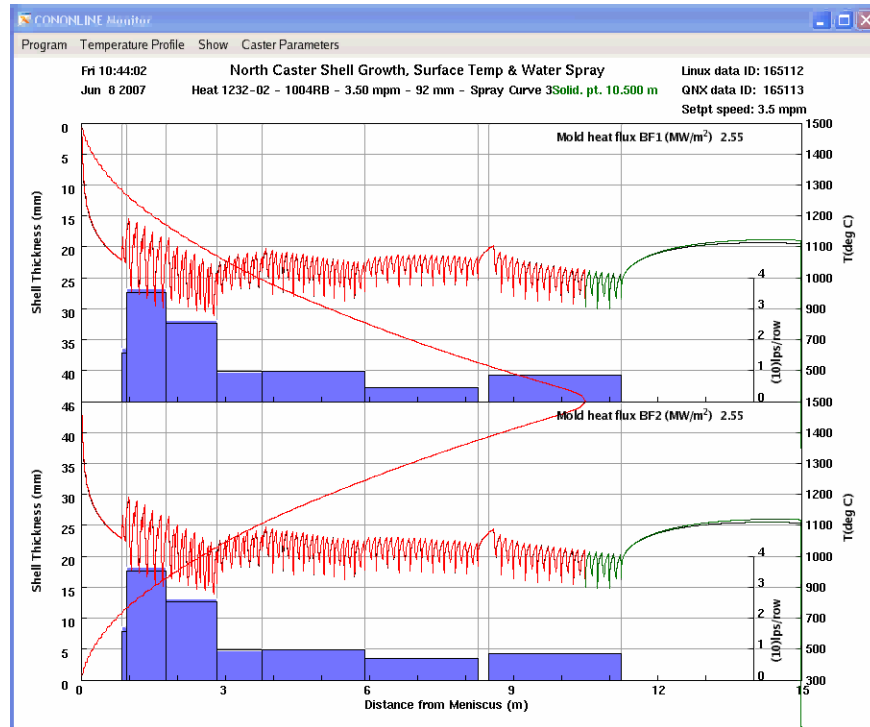
- Run setpoints for $\pm 15\%$, $\pm 30\%$ of estimated heat flux
- Interpolate setpoints in first three zones based on mold exit temperature
- Keep standard setpoints for last four zones



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MHRR Change: PI Controller, MET-dependent Setpoints

Sped up 10x



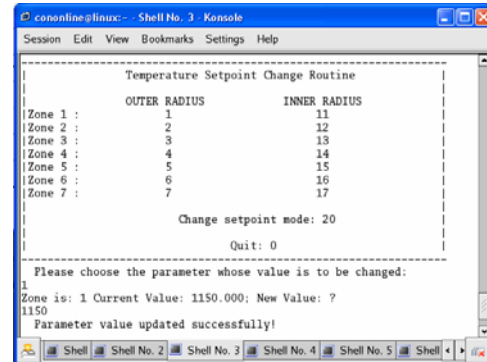
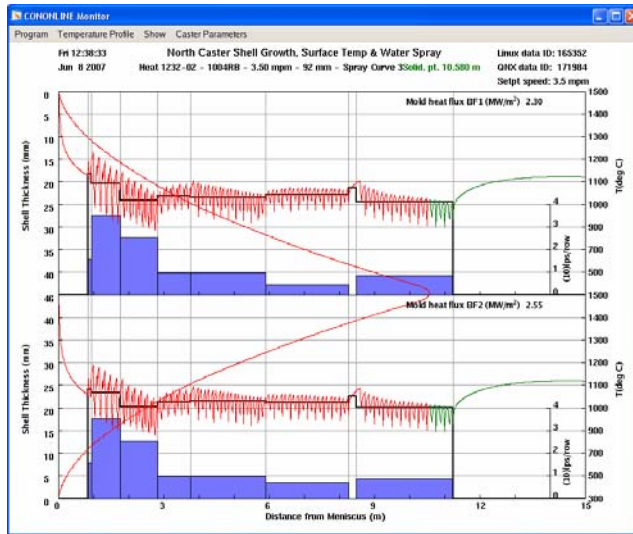
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Organizing Setpoints

- First method
 - Calculated from spray tables
 - Stored as 2D index: speed and pattern
 - Setpoints linearly interpolated with casting speed
- Current method
 - Calculated from spray tables
 - Stored as 3D index: speed, pattern, mold exit temperature
 - Typical casting speed used to calculate setpoint
 - Allowing for different mold exit temperatures avoids over-responding at top of caster
- Next method
 - Stored as temperature setpoints
 - Allow for operator to change setpoints online

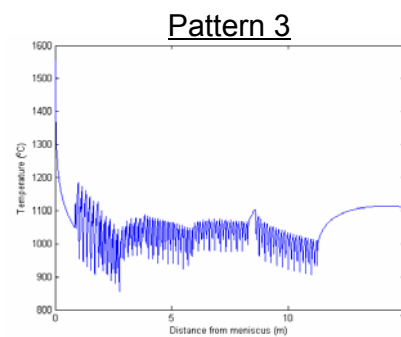
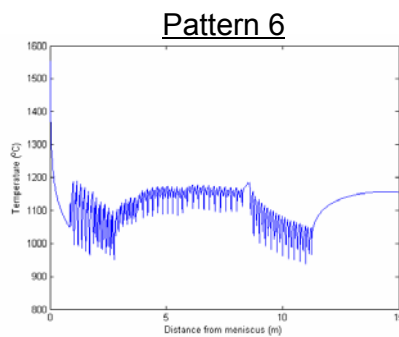
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Shared Memory Setpoints



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Simulation: Spray Pattern Change

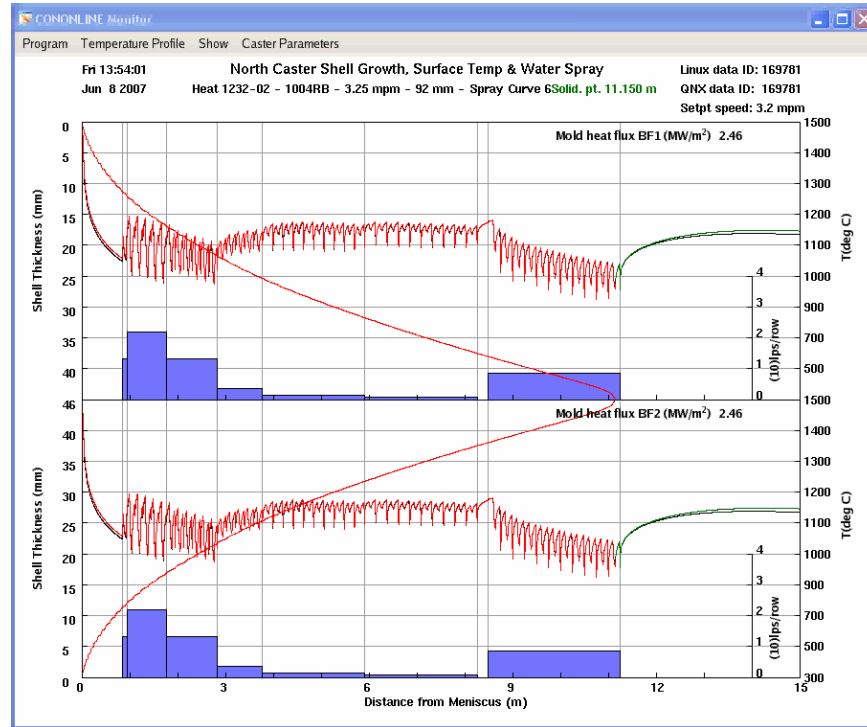


- Change from pattern 6 (low-sprays, high temperatures) to pattern 3 (high-sprays, low temperatures) at 30 seconds
- Compare
 - Casting-speed-based controller
 - Model-based PI controller: speed-independent setpoints, interpolated by mold exit temperature

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Spray Pattern Change: Casting-speed-based Controller

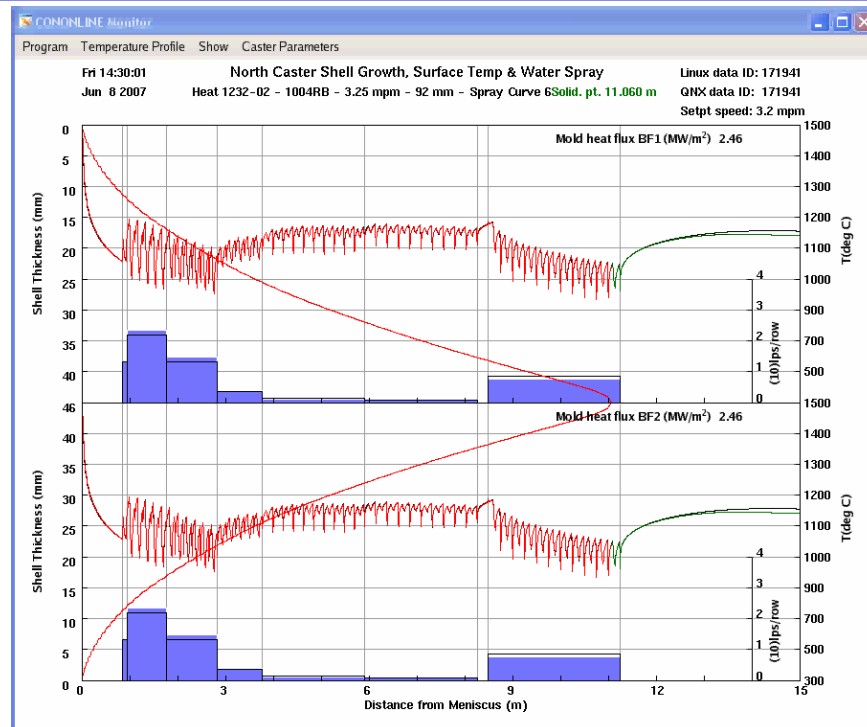
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Spray Pattern Change: Model-based Controller

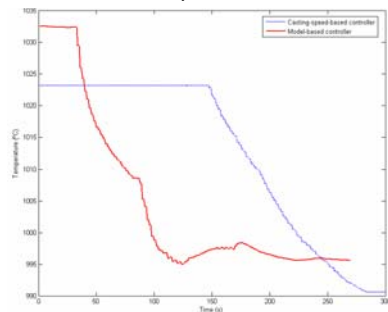
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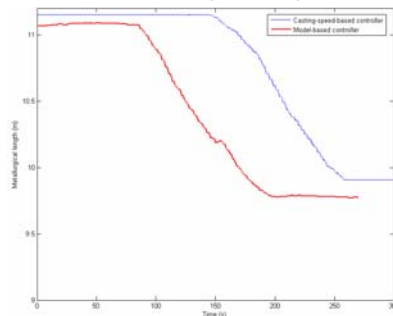
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Spray Pattern Change: Comparison

Inner radius surface temperature at end of containment



Metallurgical length



- Spray pattern changes at 30 seconds from 6 (low sprays) to 3 (high sprays)
- Model-based controller tracks temperature more quickly than casting-speed-based controller
- However, metallurgical length still takes time to respond to spray change

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Conclusions

- Control objectives must be carefully considered
 - CONONLINE can track temperature setpoints well, but this does not guarantee metallurgical quality or prevention of whales (ML control)
 - Choice of temperature setpoints is important, and is not always obvious
- Further work:
 - Incorporate heat transfer coefficients from lab experiments and plant measurements to improve accuracy
 - Huan's work
 - Develop off-line system to model plant separately from software sensor and study effect of differences
 - Improved control logic
 - Optimal or adaptive control?

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